



# The Inhomogeneous MUSIG Model: Validation and Comparison with TOPFLOW experiments

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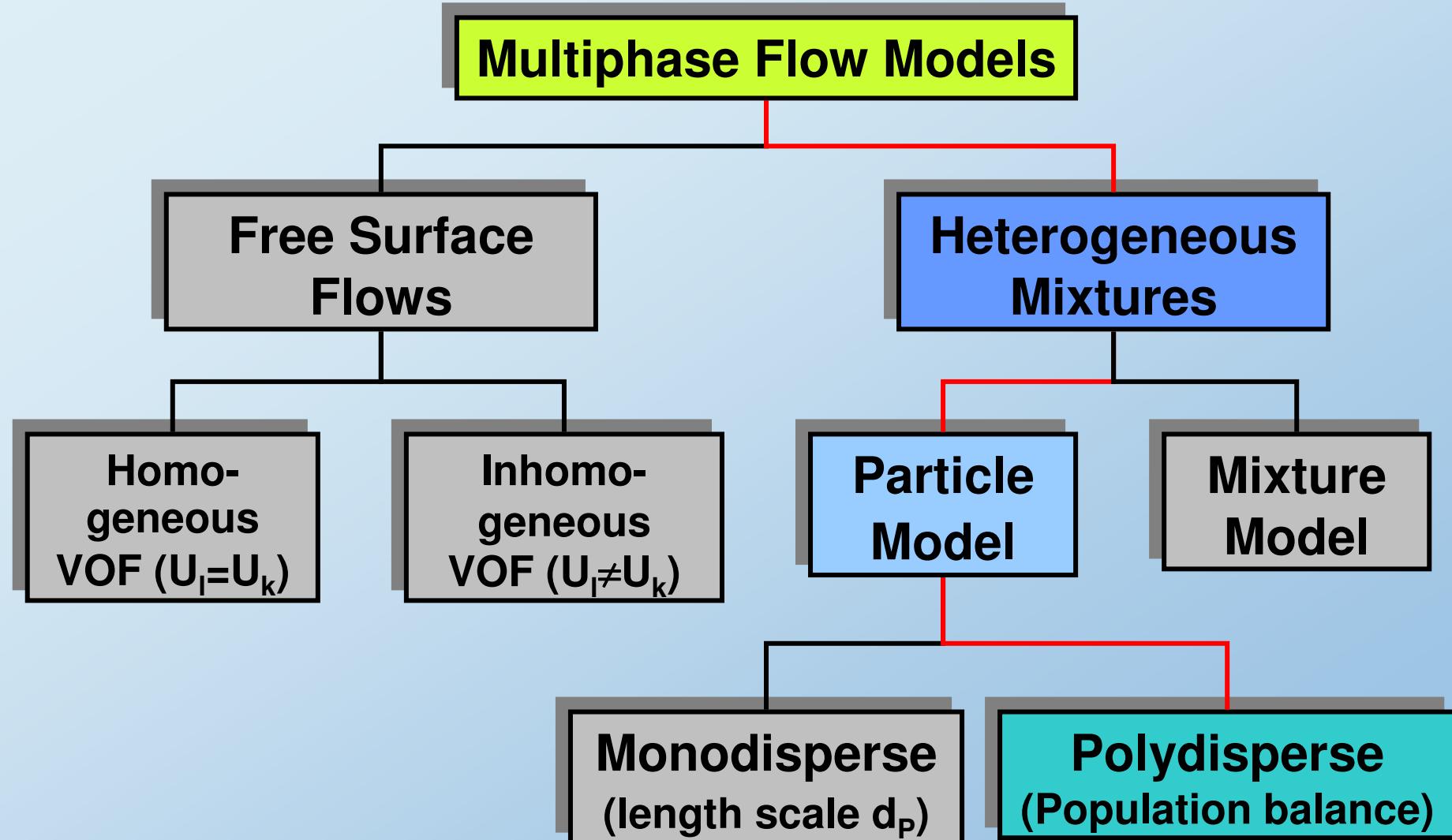
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- **Introduction**
- **The testcase TOPFLOW-074**
- **Validation tests and comparison with experimental results**
- **Summary & Conclusions**

# Modeling Strategies



# Polydispersed bubbly flow caused by breakup & coalescence

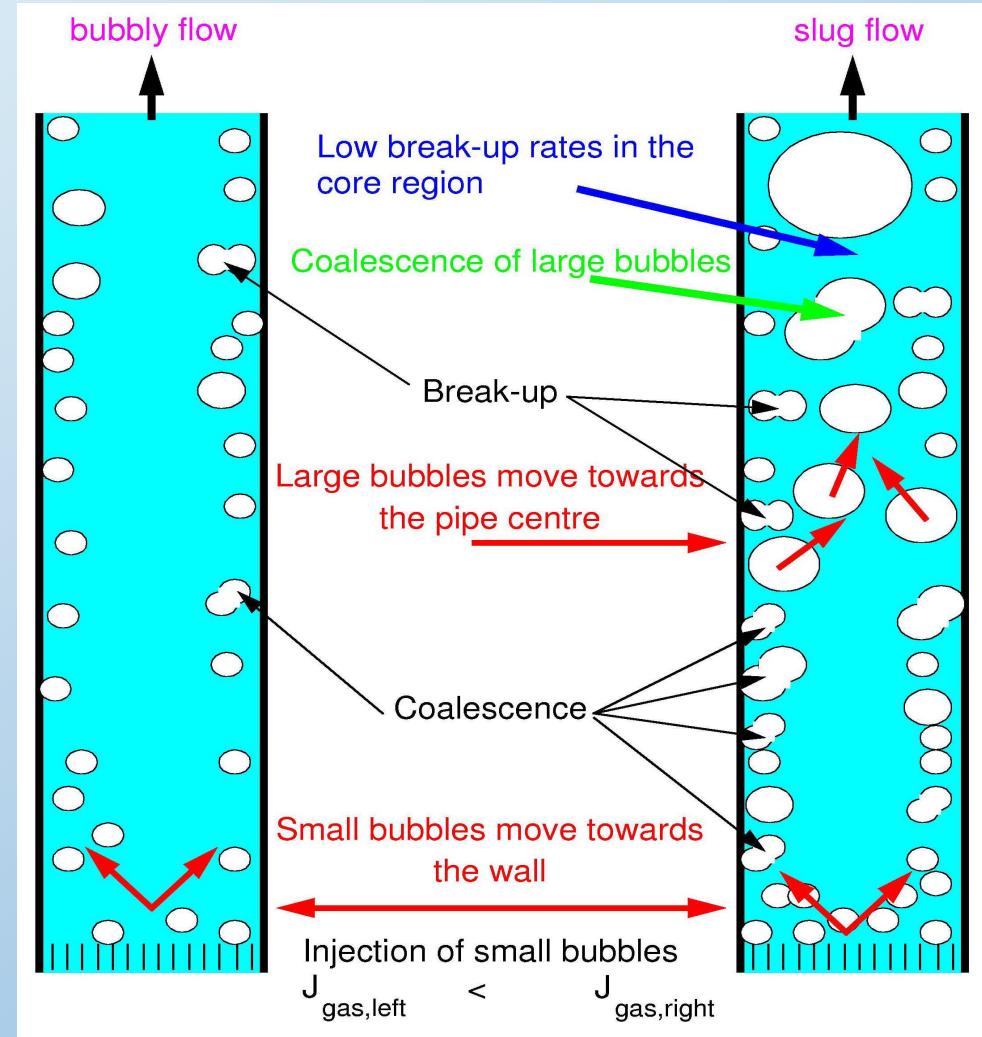


Transition from disperse bubbly flow to slug flow:

- **coalescence of bubbles**
- turbulent bubble **breakup**

**bubble size distribution;**  
**polydisperse bubbly flow**  
**counter-current radial motion**  
**of small and large bubbles;**  
**more than one velocity field**

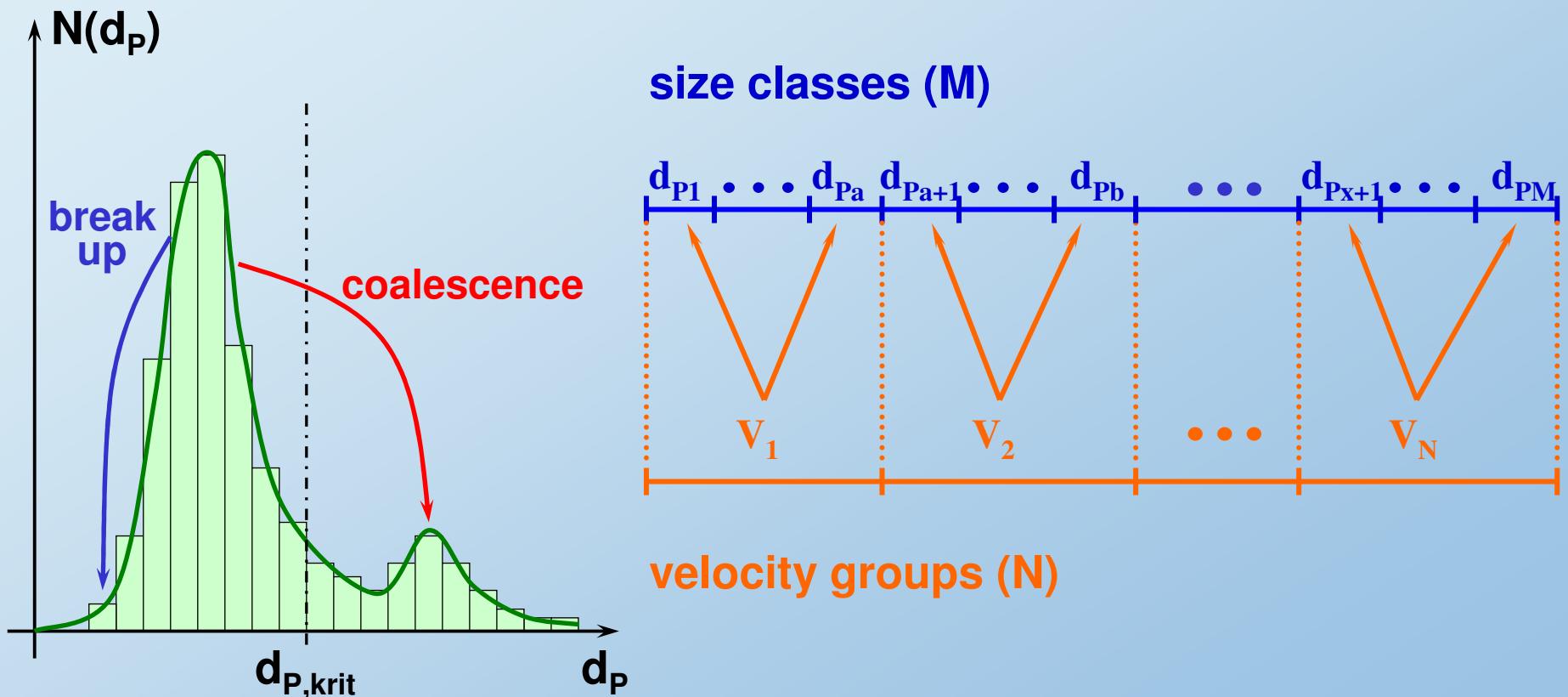
**new population balance model (inhomogeneous MUSIG)**



# The inhomogeneous MUSIG model



- momentum equations are solved for **N** gas phases (vel. groups)
- size fraction equations for **M** bubble size classes in each vel. group
- bubble coalescence and break-up over all **NxM** MUSIG groups



## Inhomogeneous MUSIG model solves for:

- N           **volume fraction equations**
- N+1       **momentum equations**
- (>) 2     **turbulence model equations**
- NxM       **size fraction equations**

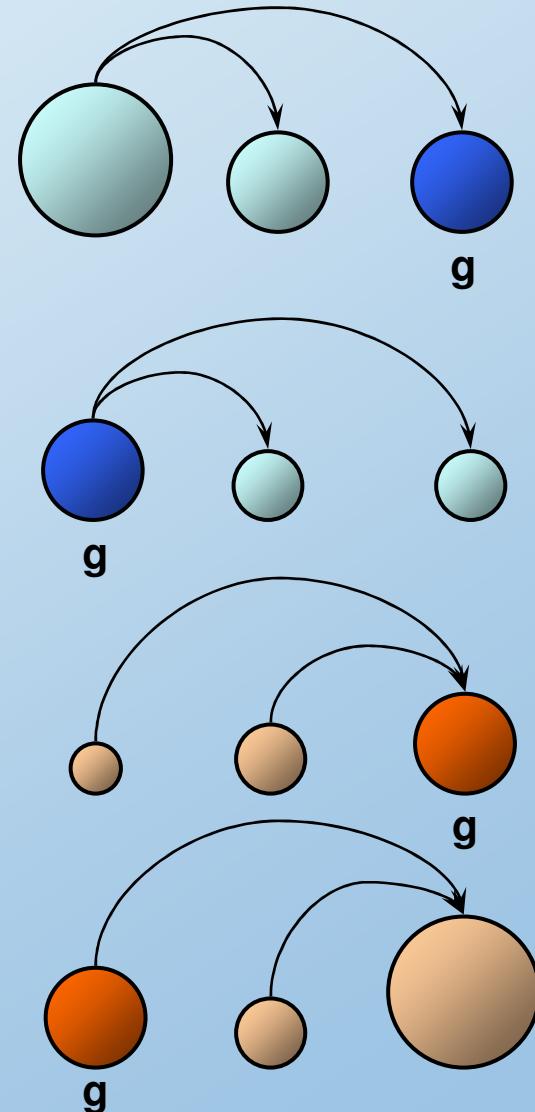
$$\frac{\partial}{\partial t} (\rho_d r_{dg}) + \frac{\partial}{\partial x^i} (\rho_d r_{dg} u_{g,j}^i) = S_g \quad g=1, \dots, N \cdot M \quad j=1, \dots, N$$

$$r_d = \sum_{g=1}^{N \cdot M} r_{dg} \quad , \quad f_{dg} = \frac{r_{dg}}{r_d} \quad , \quad \sum_{g=1}^{N \cdot M} f_{dg} = 1 \quad , \quad \sum_{g=1}^{N \cdot M} S_g = 0$$

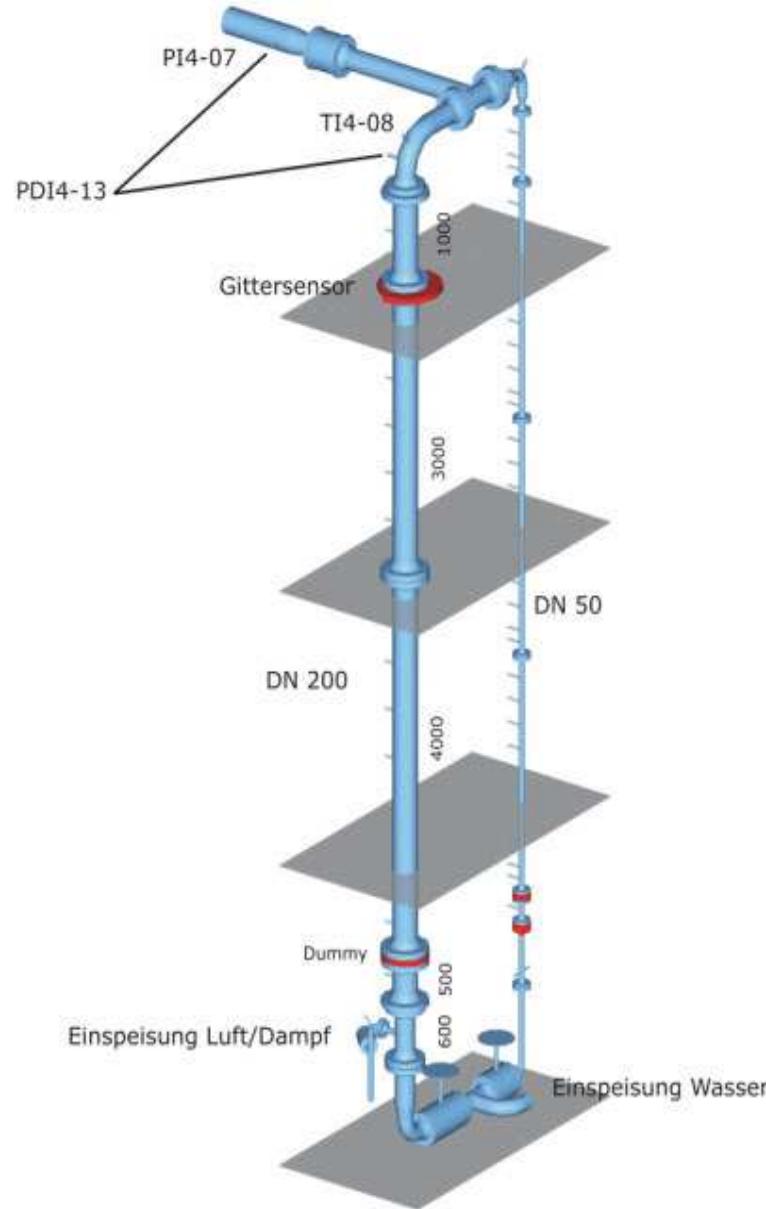
# The inhomogeneous MUSIG model



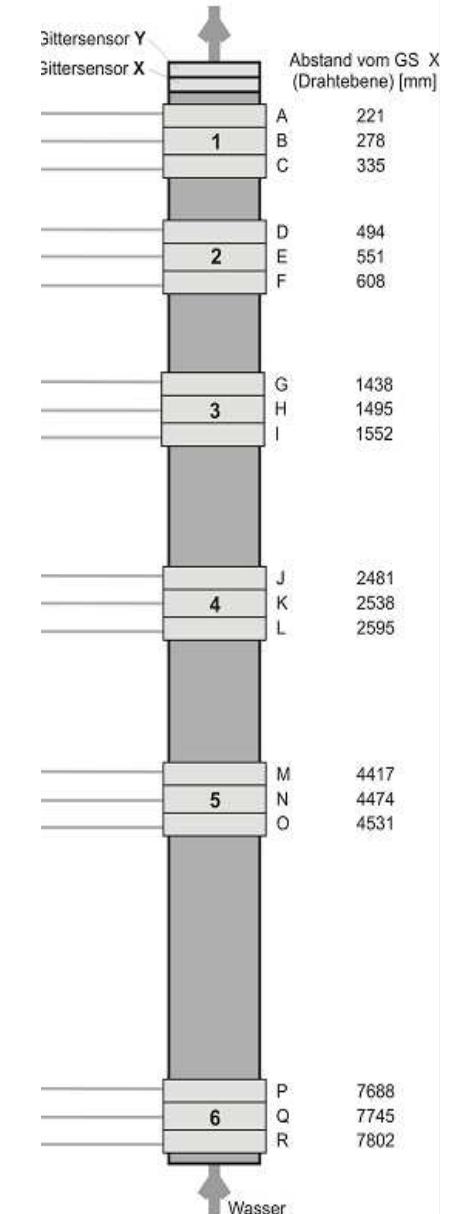
$$\begin{aligned}
 S_g &= \rho_d \underbrace{\sum_{h=g+1}^{N \cdot M} B_{gh} r_{dh}}_{\text{breakup birth}} \\
 &\quad - \rho_d r_{dg} \underbrace{\sum_{h=1}^{g-1} B_{gh}}_{\text{breakup death}} \\
 &\quad + \frac{1}{2} \rho_d \underbrace{\sum_{h=1}^g \sum_{i=1}^g C_{hi} r_{dh} r_{di} X_{g \leftarrow hi} \frac{m_h + m_i}{m_h m_i}}_{\text{coalescence birth}} \\
 &\quad - \rho_d r_{dg} \underbrace{\sum_{h=1}^{N \cdot M} C_{gh} \frac{r_{dh}}{m_h}}_{\text{coalescence death}}
 \end{aligned}$$



# The TOPFLOW test facility at FZR



- FZR TOPFLOW test facility with DN200
- gas injection through 72 x 1mm Ø wall injection holes
- $J_W=1.017 \text{ m/s}$   
 $J_G=0.0368 \text{ m/s}$
- $r_G=3.49\%$   
(mean gas volume fraction)



# 3x7 inhomogeneous MUSIG simulations for TOPFLOW-074



- **3x7 MUSIG model** applied to TOPFLOW-074 testcase with :  
**N=3 velocity groups** and  
**M=21 size classes** (7 in each group)
  - overall bubble diameter range  $d_p=0,\dots,13\text{mm}$
  - equal diameter discretization ( $\Delta d_p=0.619\text{mm}$ )
  - **Air1 vel. group :**  $d_{p,\min}=0.31\text{ mm} ; d_{p,\max}=4.02\text{mm}$
  - **Air2 vel. group :**  $d_{p,\min}=4.64\text{ mm} ; d_{p,\max}=8.36\text{mm}$
  - **Air3 vel. group :**  $d_{p,\min}=8.98\text{ mm} ; d_{p,\max}=12.69\text{mm}$

# 3x7 inhomogeneous MUSIG simulations for TOPFLOW-074



5 different simulations with 3x7 MUSIG model:

No.	Grid level	No. of elements	$C_{TD}$	comment
1	2	32.000	1.0	reference case
2	4 (mod.)	260.442	1.0	grid refinement above the point of gas injection ( $z=0.0$ $z=8.0m$ ; expanding mesh)
3	4 (mod.)	260.442	1.0	inlet BC initialization with $u$ , $v$ , $w$ , $k$ , $\omega$ from fully developed single-phase flow
4	4 (mod.)	260.442	1.0	changed gas inlet bubble size distribution
5	4 (mod.)	260.442	0.5	reduced turbulent dispersion

## Cases 1-3 and 5:

- inlet nozzle injection

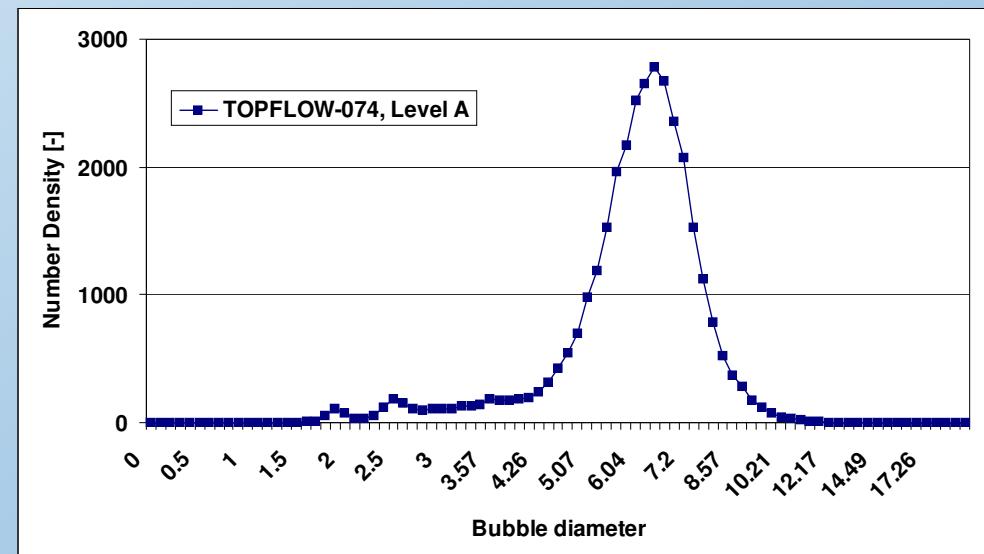
- 80% of VF in class 7 (Air1)
- 20% VF in Air1, Air2, Air3

equally distributed over  
all remaining size classes

## Case 4:

- inlet nozzle injection

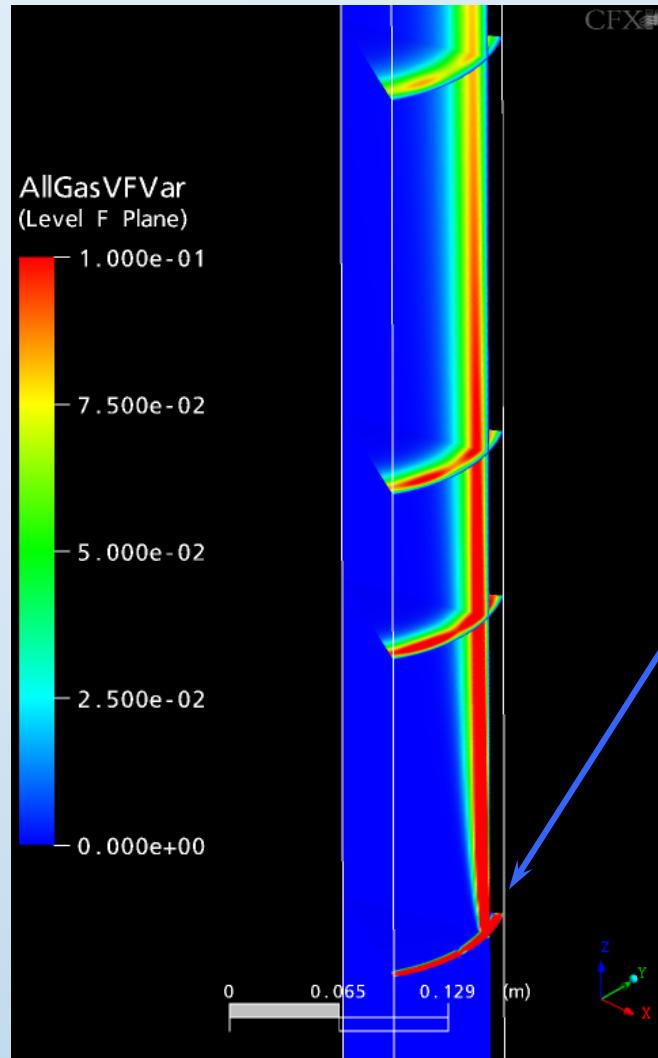
- Air1 VF = 0.844% of VF
- Air2 VF = 88.72% of VF
- Air3 VF = 10.93% of VF



# Case 4: 3x7 inhomogeneous MUSIG simulations for TOPFLOW-074



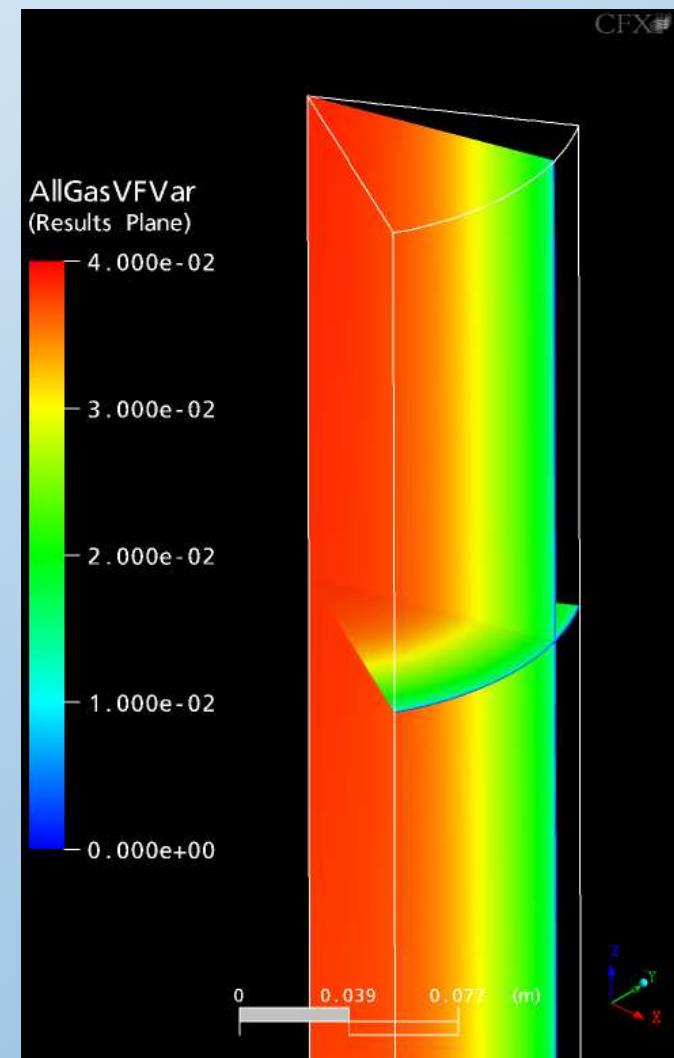
Inlet level



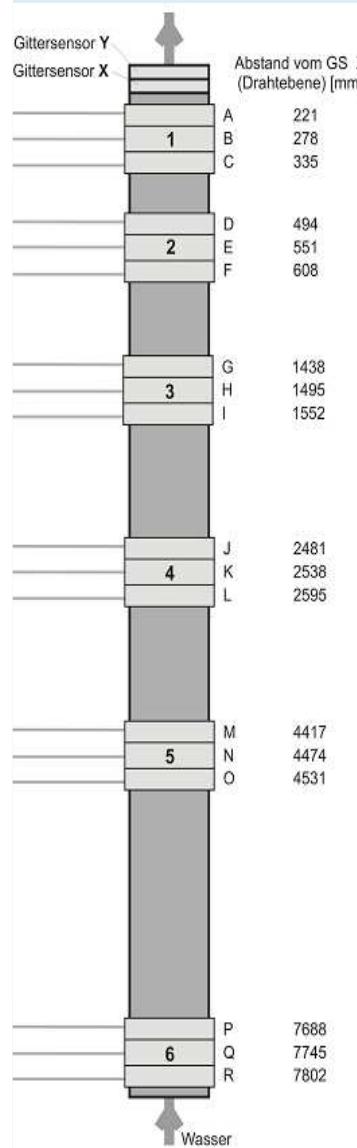
level F

- TOPFLOW-074 best results obtained in Case 4
- near wall gas injection at  $z=0.0\text{m}$
- level R results show core peak in air VF profiles

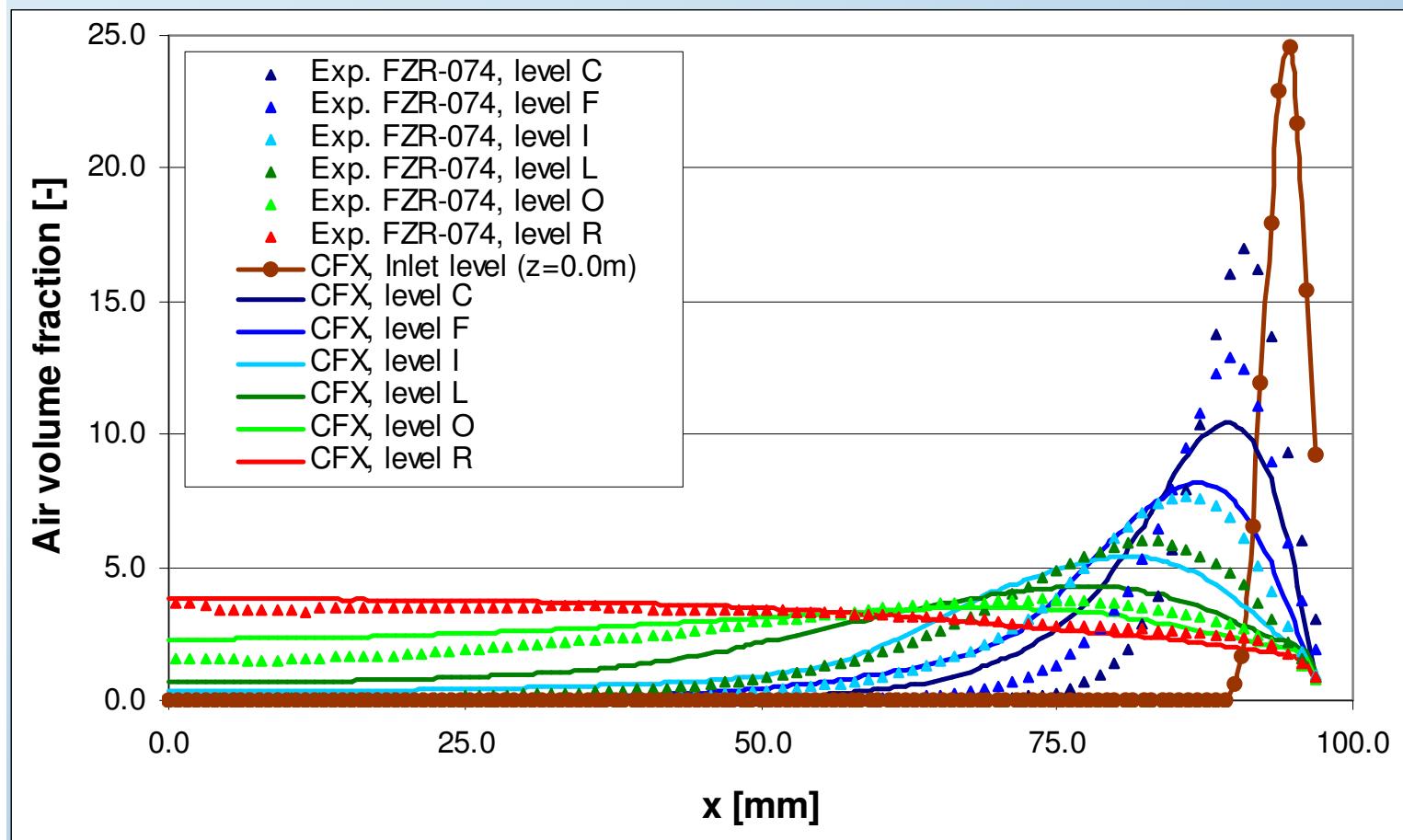
level R



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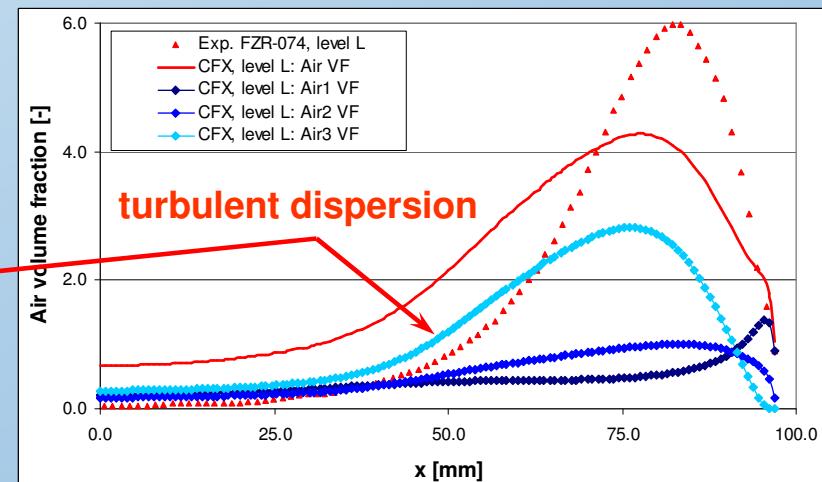
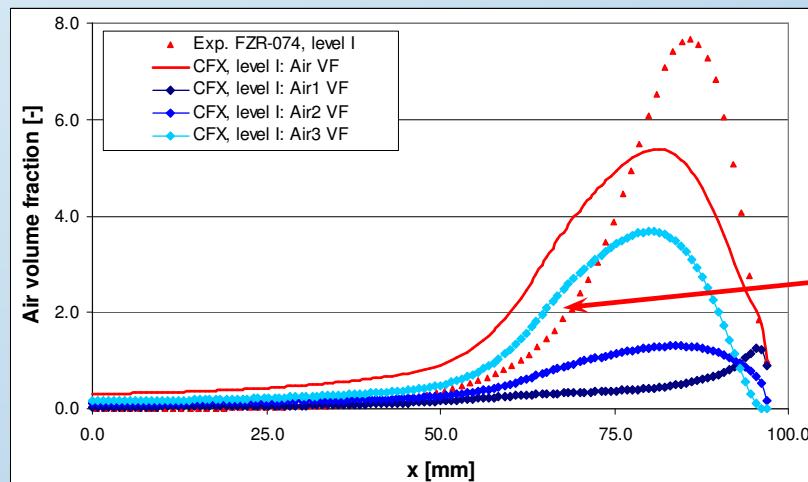
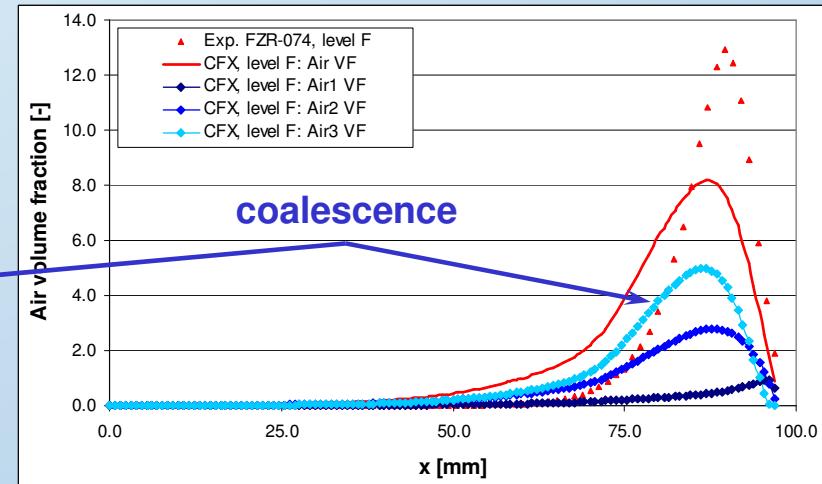
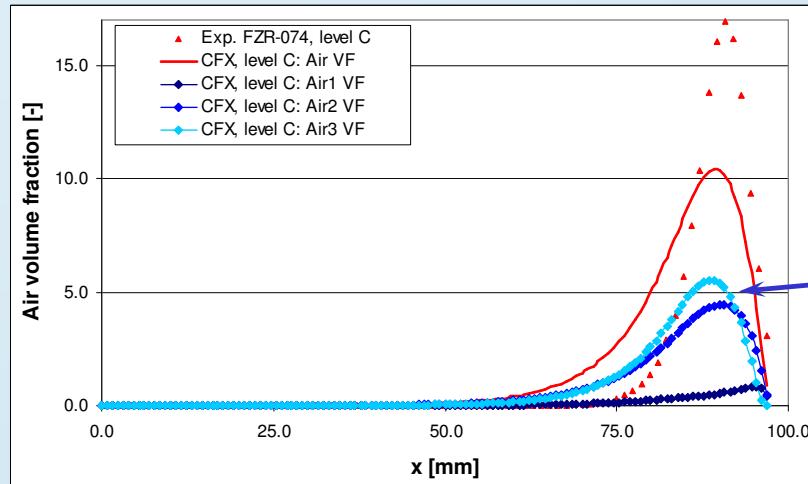
- good agreement at levels L through R
- too fast spreading of the bubble plume from inlet



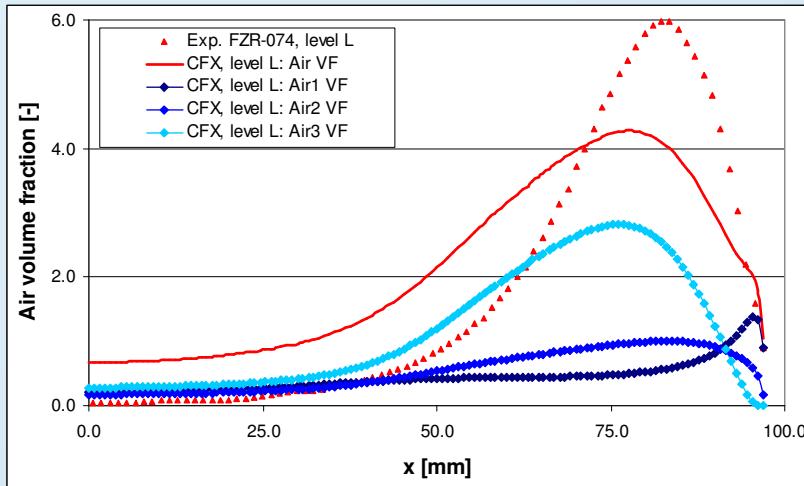
# Case 4: 3x7 inhomogeneous MUSIG simulations for TOPFLOW-074



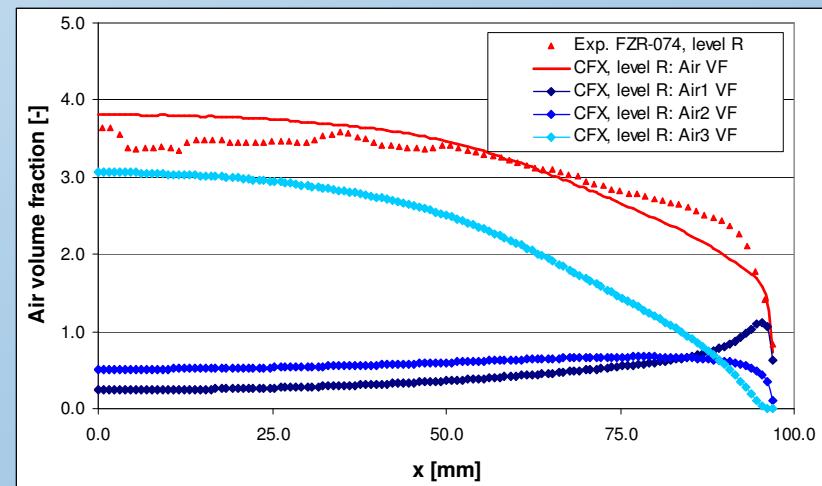
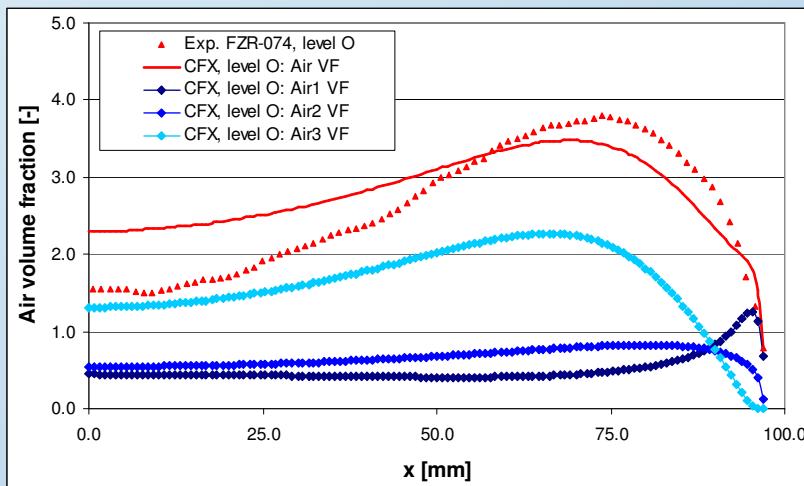
level C ( $z=0.335\text{m}$ ) to level L ( $z=2.595\text{m}$ )



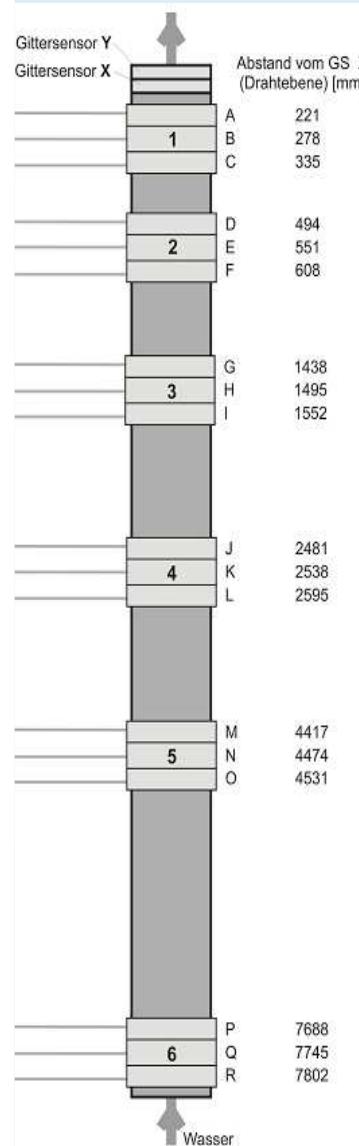
# Case 4: 3x7 inhomogeneous MUSIG simulations for TOPFLOW-074



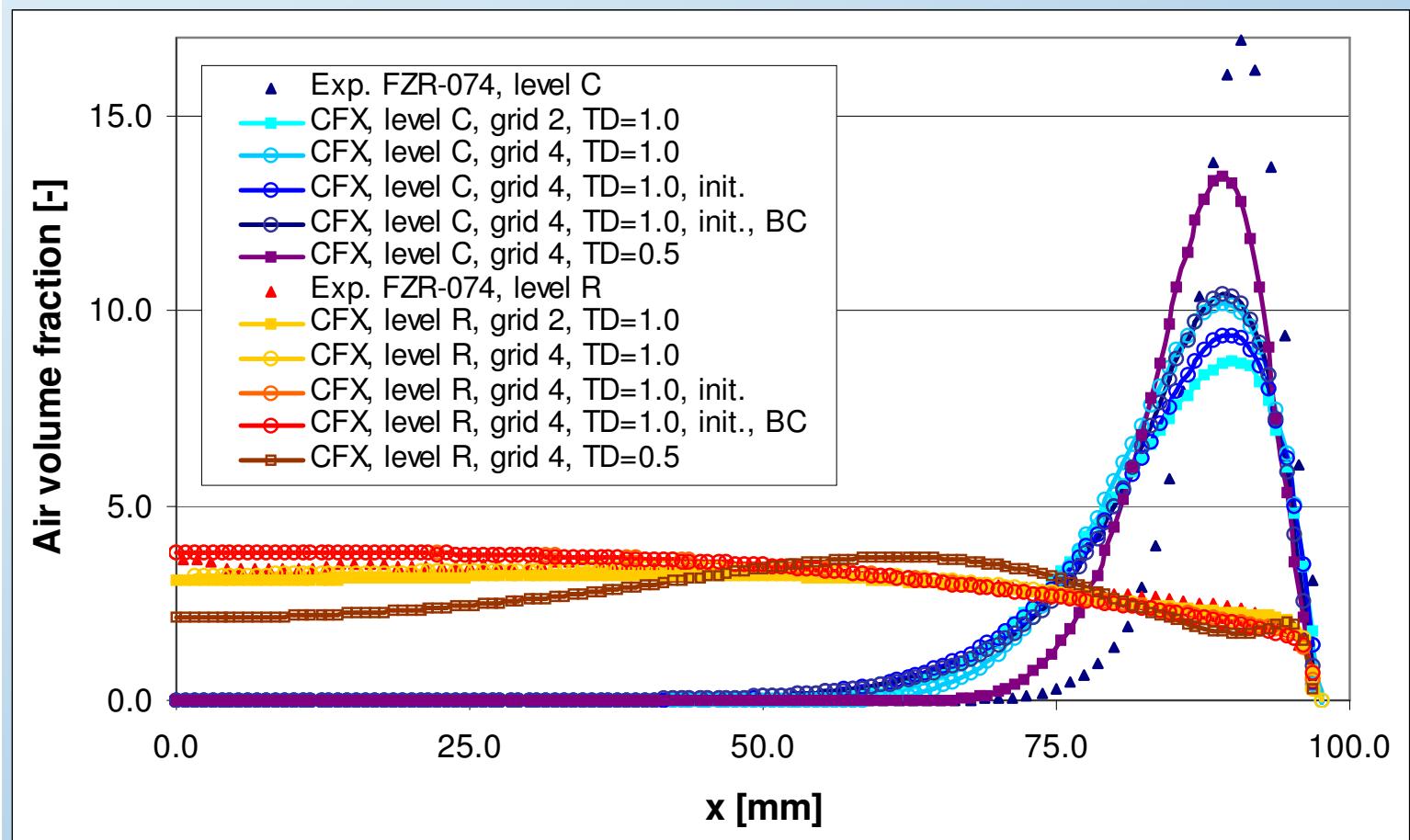
- Air VF at level L ( $z=2.595\text{m}$ ), level O ( $z=4.531\text{m}$ ) and level R ( $z=7.802\text{m}$ )
- agreement with experiments improves with increasing height
- good prediction of radial demixing processes for different bubble size classes



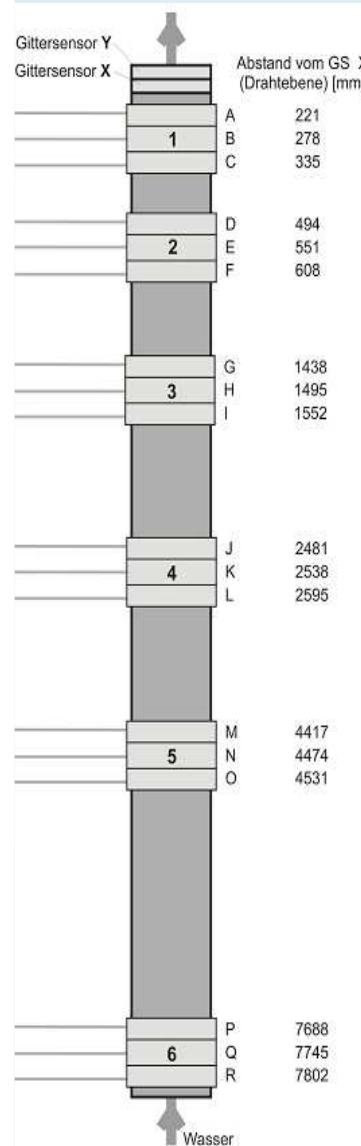
# Overall Comparison of different Validation Tests



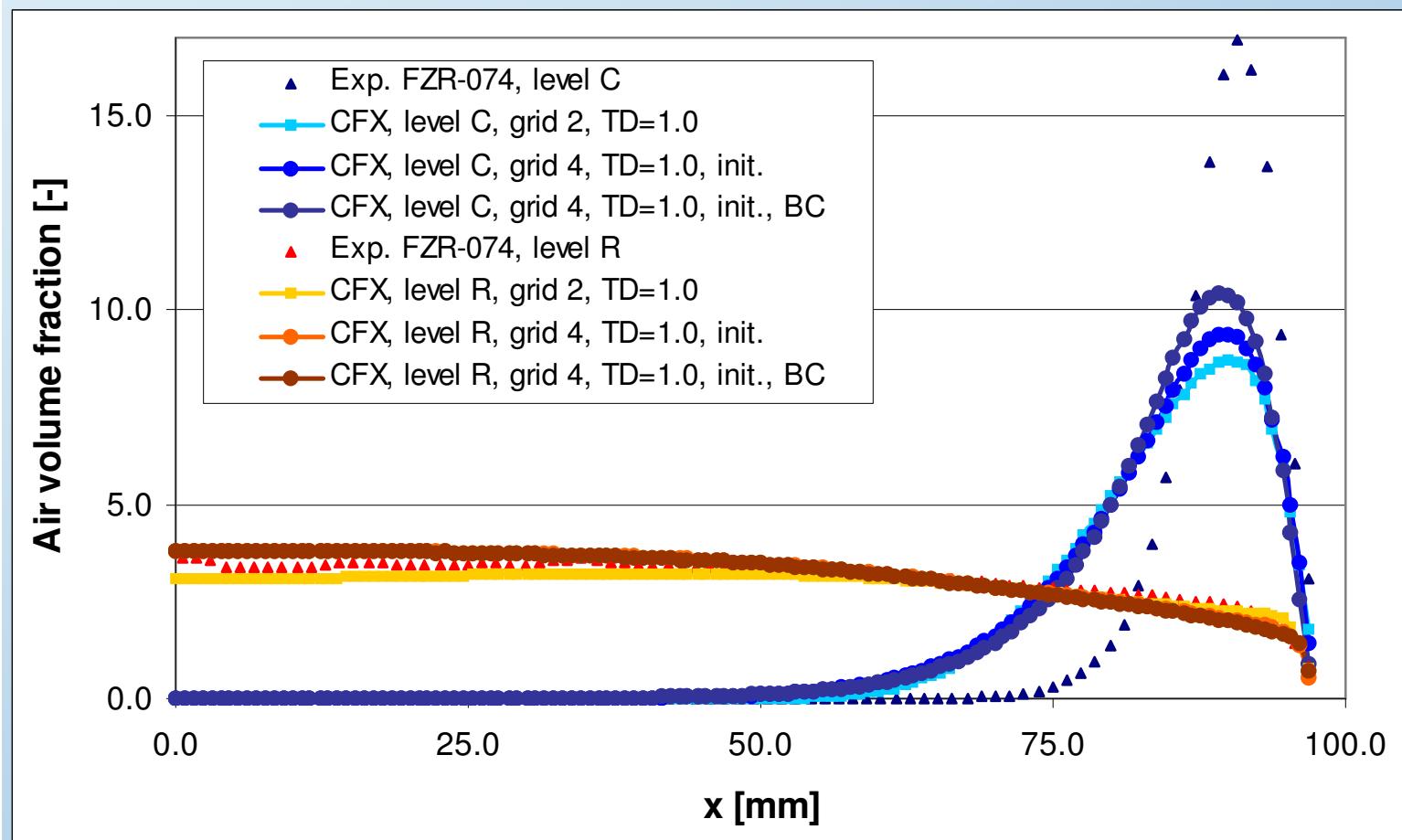
- C and R level results for Cases 1- 5



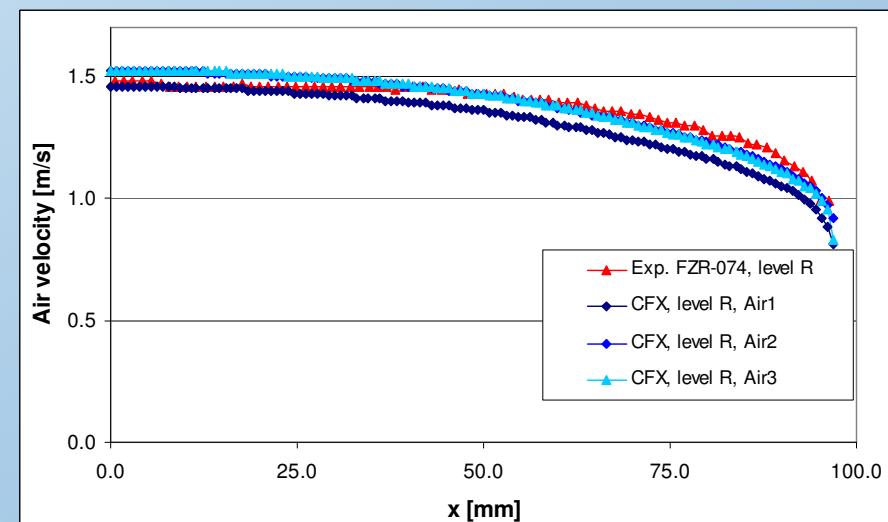
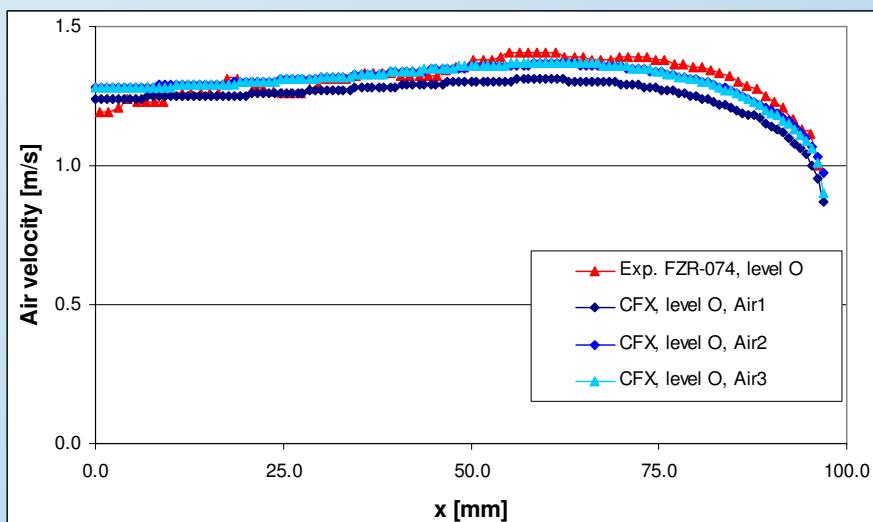
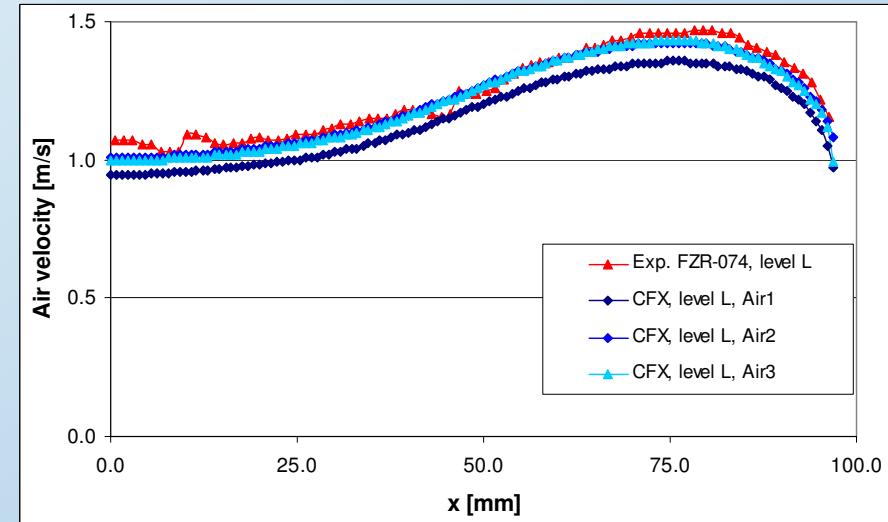
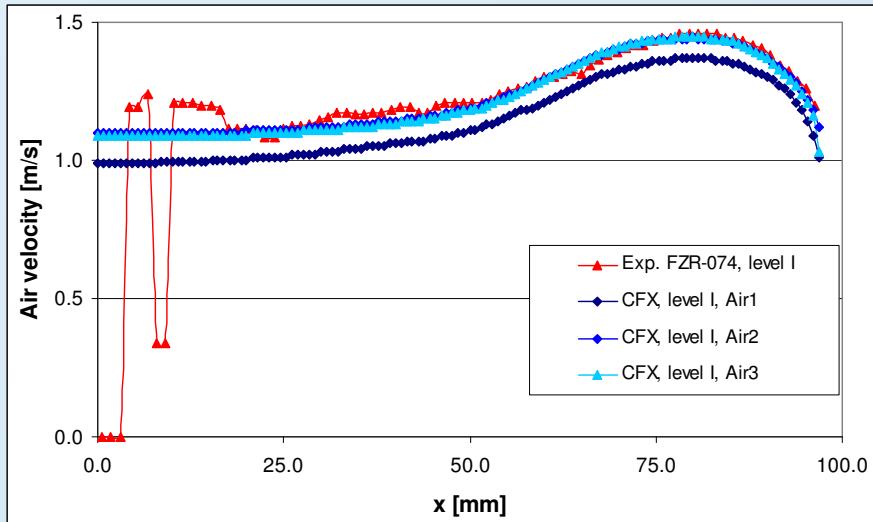
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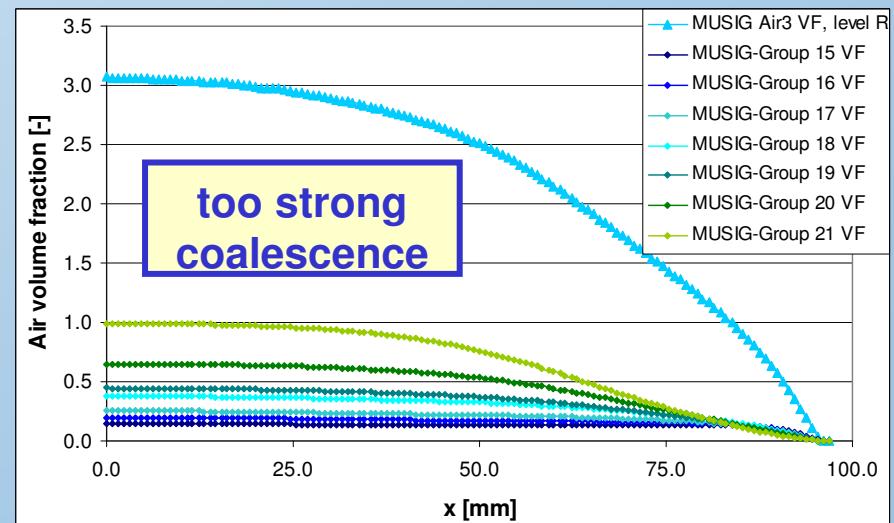
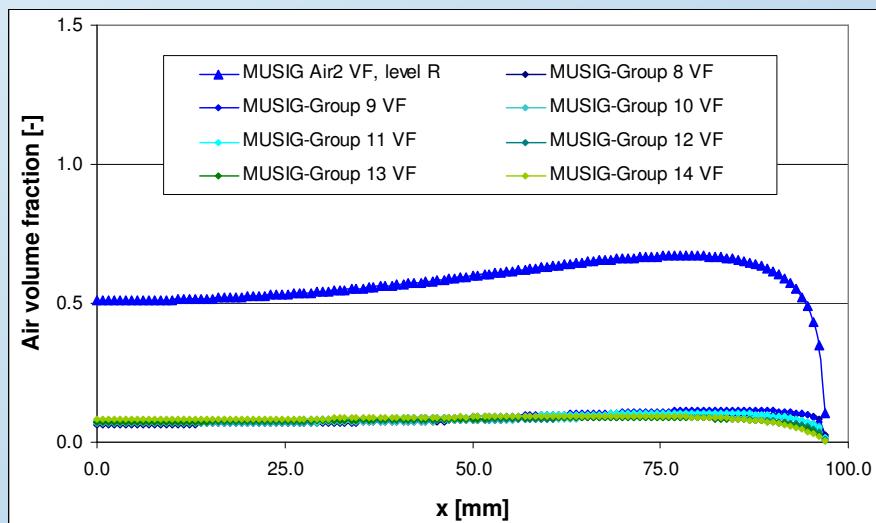
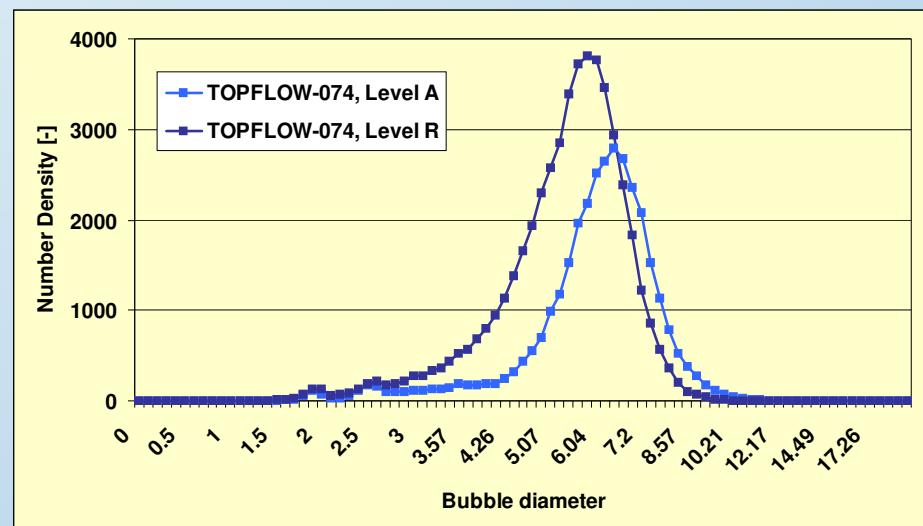
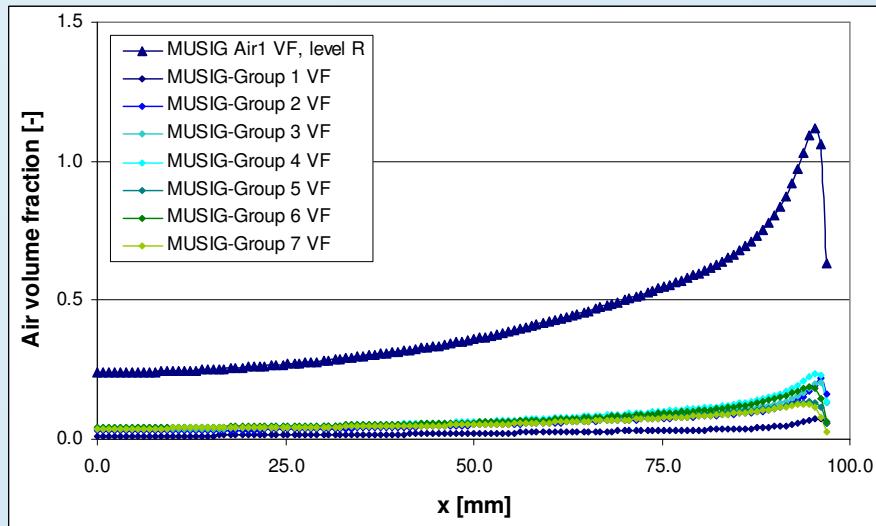
- C and R level results for Cases 1, 3 and 4



# Case 4: Velocity Profiles I R Level Comparison with Exp.



# Case 4: Evolution of Bubble Size Distribution – Level R



# Summary & Conclusions



- New population balance model in CFX-5:  
**inhomogeneous NxM MUSIG model**
- Validation on TOPFLOW-074:
  - radial demixing of differently sized bubbles
  - good agreement for air void fraction and velocity profiles at higher pipe elevations
  - too fast spreading of near wall bubble plume
  - too strong coalescence (imbalance with breakup)
- Validation for broader range of flow conditions necessary   TOPFLOW test matrix
- Revision of breakup & coalescence models
- Future extension of inhomogeneous MUSIG model to condensation & boiling